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## Study on the adsorption of lead(II) in wastewater by hazelnut shell powder

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### ABSTRACT

In order to study the adsorption mechanism of hazelnut shell powder on Pb<sup>2+</sup>, This work studied on kinetic adsorption properties and isothermal adsorption property of Pb<sup>2+</sup> in hazelnut shell powder, and the thermodynamic analysis was carried out. The results show that the Pseudo-second-order model is suitable for the adsorption of Pb<sup>2+</sup> on HS, the maximum adsorption capacity obtained by Langmuir model is very close to the actual value, and maximum adsorption capacities were 65.66mg/g. The process of hazelnut shell powder adsorbent of Pb<sup>2+</sup> was an exothermic process. © 2016 Trade Science Inc. - INDIA

### KEYWORDS

Hazelnut shell powder;  
Biosorption;  
pb(II);  
Kinetics;  
Isothermal adsorption.

### INTRODUCTION

Heavy metal pollution is irreversible, they do not likely organic pollutants after a period of time can be achieved by biological degradation, and they can never be automatically reduced to a safe concentration range. The only effective way to reduce the pollution of heavy metal ions is to remove the heavy metal ions from water. Domestic and foreign scholars have focused on the research of forestry and agricultural residues such as straw, peel, bark, nut shell to prepare the adsorbent for the adsorption of heavy metal ions<sup>[1-5]</sup>. The hazelnut shell waste rich in cellulose, hemicellulose, lignin is very suitable for the adsorption of metal elements in the water. In this work, the adsorption mechanism of systematic removal of Pb<sup>2+</sup> of hazelnut shell adsorbent was studied and the effects of pH, temperature, adsorption

time and adsorbate concentration on the adsorption were investigated. The adsorption behavior of Pb<sup>2+</sup> in water was analyzed by using Langmuir, Freundlich isothermal adsorption model, thermodynamic model, pseudo-first-order kinetic model and pseudo-second-order kinetic model.

### EXPERIMENTS

#### Instrumentation and reagents

Hazelnut shell produced in Liaoning Xiuyan, 70 °C dry and crushed 80 mesh sieve, later put in the dryer. The product was named HS.

Atomic absorption spectrophotometer (AAAnalyst 200, PerkinElmer) gas-bath Constant temperature oscillator (THZ-92A SH1717).

#### Adsorption experiment method

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A certain amount of hazelnut shell powder was added in the 100ml erlenmeyer flask, then add 20ml a certain concentration of  $Pb^{2+}$  standard solution, adjusting pH value, adsorption of a certain time in a certain temperature ( $30^{\circ}C$ ,  $40^{\circ}C$ ,  $50^{\circ}C$ ,  $60^{\circ}C$ ) oscillated adsorption. The  $Pb^{2+}$  concentration in the filtrate was determined by the flame atomic absorption spectrophotometer, and calculate the adsorption capacity (1) and adsorption rate (2).

$$q = \frac{(c_0 - c_e)V}{m} \quad (1)$$

$$\text{Adsorption\%} = \frac{c_0 - c_e}{c_0} \quad (2)$$

Where  $c_0$  and  $c_e$  are the initial concentration and equilibrium concentration (mg/L);  $m$  was the mass of the adsorbent used for adsorption experiment (mg);  $V$  was the volume of adsorbate solution (mL).

## RESULTS AND DISCUSSION

### The effect of pH on adsorption property

From the data in Figure 1, when the initial pH increased from 2 to 4, the adsorption rate of HS on  $Pb^{2+}$  was increased from 20.87% to 98.12%. When  $pH > 4$ , the adsorption tends to be stable. This is due to the hazelnut shell containing -NH, -OH, R-C-NH<sub>2</sub>, C=O, COO<sup>-</sup> groups. The adsorption activity is surrounded by proton, and in high pH value of the solution, adsorption activity is exposed, so when the solution pH was high up, HS on  $Pb^{2+}$  adsorption per-

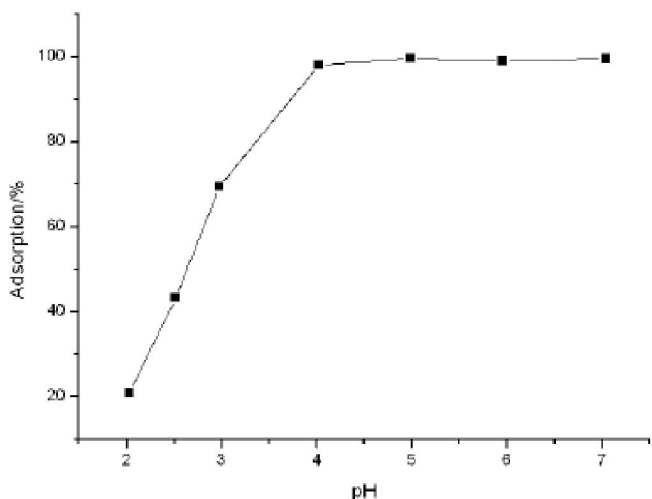


Figure 1 : Effect of pH on the adsorptivity

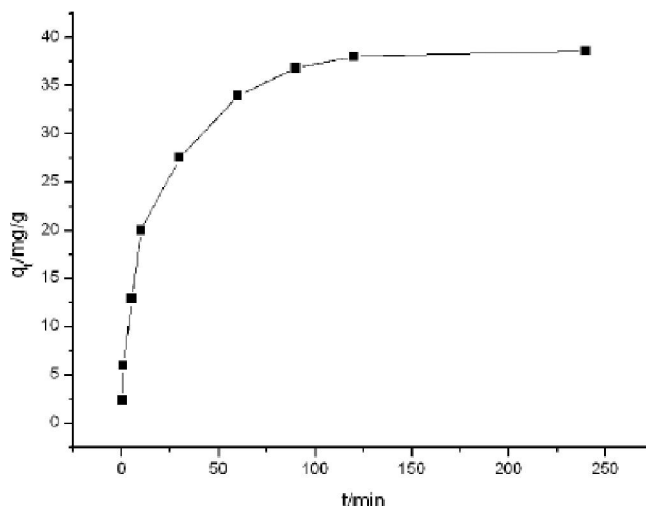


Figure 2 : Effect of time on adsorption

formance improved significantly.

### Adsorption kinetics

Kinetic and equilibrium models were employed to analyse the data of the complete adsorption process to better understand the  $Pb^{2+}$  sorption characteristics by HS. From Figure 2, we can see that the adsorption rate of HS on  $Pb^{2+}$  is very fast, and 120 min contact time was considered to be adequate for the adsorption. We used pseudo-first-order kinetic model (3), pseudo-second-order kinetic model (4), the adsorption process was simulated to analyze the relationship between adsorption time and adsorption capacity, fitting results are shown in Figure 3, the corresponding parameters are listed in TABLE 1.

$$\ln(q_e - q_t) = \ln q_e - k_1 t \quad (3)$$

$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{1}{q_e} t \quad (4)$$

Where  $q_e$  represents the calculated values of the adsorption capacity of HS at equilibrium (mg/g);  $q_t$  (mg/g) was the adsorption amount at time  $t$  (min);  $K_1$  ( $\text{min}^{-1}$ ),  $K_2$  ( $\text{g}/(\text{mg}\cdot\text{min})$ ) are the rate constants of pseudo-first-order and pseudosecond-order kinetics equations, respectively.

It can be seen that the correlation between the pseudo-second-order kinetic model fitting results is higher than that of the pseudo-first-order kinetic model, and the linear correlation coefficient is more than 0.999. And the saturated adsorption capacity

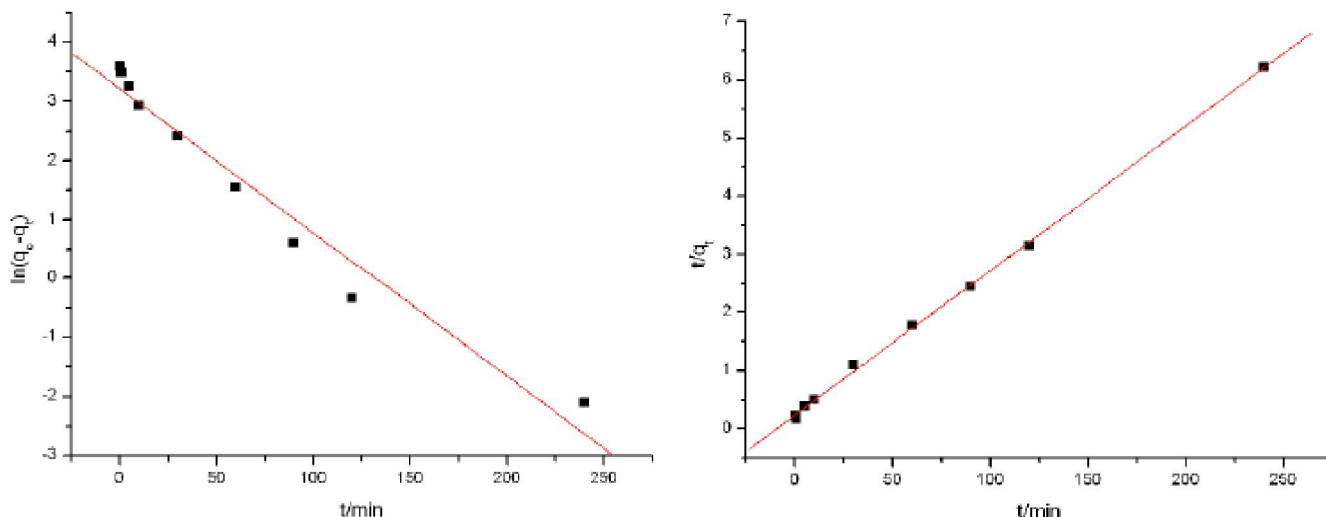


Figure 3 : a. Pseudo-first-order kinetics plots for the adsorption of pb<sup>2+</sup> on HS b Pseudo-second- order kinetics plots for the adsorption of pb<sup>2+</sup> on HS

TABLE 1 : Kinetic parameters for the removal of MG by HS

Quasi first order equation					Quasi two order equation				
qe, exp	k <sub>1</sub>	qe,cal	Relative error/%	R <sup>2</sup>	k <sub>2</sub>	qe,cal	Relative error/%	R <sup>2</sup>	
38.57	0.024	24.98	35	0.9625	0.0026	40.2	-4	0.9991	

obtained by the pseudo-second-order kinetic model is very close to the experimental saturated adsorption capacity. The relative error is -4%, which indicates that the pseudo-second-order kinetic model can describe the adsorption process.

**Adsorption isothermal**

It can be seen that the adsorption capacity increases with the increase of pb<sup>2+</sup> concentration in solution, and the final equilibrium is reached. The experimental data were analyzed by using different isothermal adsorption models, and the theoretical basis of HS adsorption on pb<sup>2+</sup> could be provided. In this study, the data were fitted to the Langmuir isotherm model (5), Freundlich isothermal adsorption model (6), and the data from Figure 4a. The results are shown in Figure 4 and TABLE 3.

$$\frac{c_e}{q_e} = \frac{1}{q_m b} + \frac{c_e}{q_m} \tag{5}$$

$$\lg q_e = \lg k_F + \frac{1}{n} \lg c_e \tag{6}$$

Where q<sub>e</sub> represents the calculated values of the adsorption capacity of HS at equilibrium (mg/g); q<sub>m</sub> was the maximum adsorption capacity (mg/g); c<sub>e</sub> was adsorbed at equilibrium when the concentration (mg/

L), and b was Langmuir the isothermal adsorption equation constant (L/mg); k<sub>F</sub> was the Freundlich constant (mg/L), and n was related to the adsorption capacity.

From the linear correlation coefficient, Langmuir isothermal adsorption model was more suitable for describing the adsorption process of HS on pb<sup>2+</sup>. The saturated adsorption capacity and the measured values were very close to the Langmuir isothermal adsorption model, and the relative error was -0.7%, which indicated that the adsorption of pb<sup>2+</sup> on the HS was a single molecular layer adsorption.

**Thermodynamic analysis**

Investigated the effect of temperature on the adsorption properties, and according to the formula (7) (8) (9) calculation of the value of HS on adsorption of Pb<sup>2+</sup> on ΔG<sup>0</sup>, ΔH<sup>0</sup>, ΔS<sup>0</sup>

$$\Delta G^0 = \Delta H^0 - T\Delta S^0 \tag{7}$$

$$\ln k = -\frac{\Delta H^0}{RT} + \frac{\Delta S^0}{R} \tag{8}$$

$$k = \frac{C_a}{C_e} \tag{9}$$

Where R was a gas constant (8.314 J·mol<sup>-1</sup>·K<sup>-1</sup>); T was the thermodynamic temperature (K); k was the

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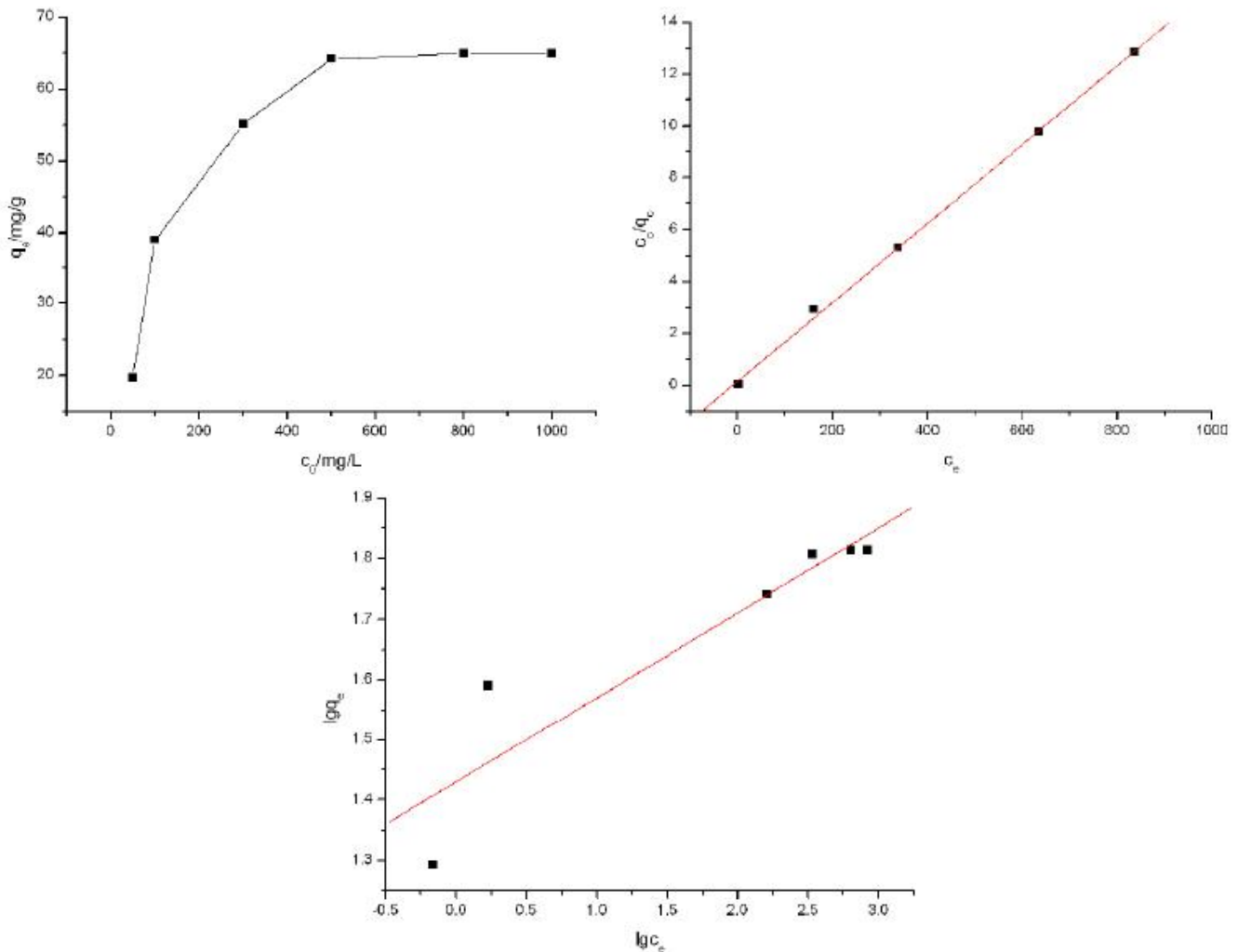


Figure 5 : a Influence of initial concentrations on the absorption capacity of HS; b Langmuir adsorption isotherm plots of HS; c Freundlich adsorption isotherm plots of HS

TABLE 2 : Langmuir, Freundlich parameters for adsorption isotherms of  $Pb^{2+}$  by HS

		Langmuir			Freundlich		
$q_{m, exp}/mg/g$	$q_m/mg/g$	$b/L/mg$	$R^2$	Relative error/%	$K_F$	$n$	$R^2$
65.02	65.66	0.108	0.9990	-0.7	26.91	7.12	0.8552

TABLE 4 : Thermodynamic parameters of  $Pb^{2+}$  adsorption of HS

Temperature (K)	Concentration mg/L	$\Delta G^0/KJ/mol$	$\Delta H^0/KJ/mol$	$\Delta S^0/J/mol\cdot K$
303	100	-10.2253	-2.001	0.024
313		-8.6066		
323		-6.3861		
333		-3.7360		

thermodynamic constant;  $c_a$  was metal ion concentrations on the adsorbent at equilibrium and  $c_e$  was the equilibrium concentration of metal ions in solution (mg/L).

The experimental results show that the  $\Delta G^0 < 0$ ,

which means that the adsorption process of HS adsorbent for  $Pb^{2+}$  is a spontaneous process. Temperature from 30°C increased to 60°C, the  $\Delta G^0$  values increased with the increase of temperature, which indicates that the high temperature is not conducive

to the hazelnut shell powder adsorption of  $Pb^{2+}$ . The adsorption reaction  $\Delta H^0 < 0$ , also shows that the adsorption was exothermic process.

### CONCLUSIONS

HS has very good adsorption performance, can adsorb  $Pb^{2+}$  in water, and it can reach the adsorption equilibrium within two hours. The saturated adsorption capacity of  $Pb^{2+}$  by Langmuir adsorption model is 65.66mg/g. In summary, HS can be used in the treatment of real waste-water, and it has achieved good results.

### REFERENCES

- [1] S.R.Shukla, Roshan S.Pai; Separation and Purification Technology, **43**, 1 (2005).
- [2] Helen M.Kalavathy, T.Karthikeyan, S.Rajgopal et al.; Journal of Colloid and Interface Science, **292**, 354 (2005).
- [3] Dandan Lu, Qilin Cao, Xiaomin Li et al.; Hydrometallurgy, **95**, 145 (2009).
- [4] M.A.P.Cechinel; Journal of Cleaner Production, **65(15)**, 3429 (2014).
- [5] Wang Qiang, Wei Shiqiang, Huang Yuming et al.; Journal of Environmental Sciences, **20**, 579 (2008).