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Different elixir and different additive way for metal ions removal efficiency of research

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ABSTRACT

This study investigated the PAC + Magnetic + PAM co-dosing and diatomite + magnetic co-dosing method for metal ions Zn^{2+} , Cu^{2+} , Pb^{+} removal in order to facilitate urban sewage treatment works in the Parameters of target dosing. © 2013 Trade Science Inc. - INDIA

KEYWORDS

Magnetic powder;
Diatomite;
Metal ions;
Removal rate.

INTRODUCTION

The stirring condition determined in the test is 300r / m × 60s in rapid stirring phase, 200R / m × 180s in slow mixing phase and 200R / m × 210s in PAM adding phase, PAC and diatomite should be added in rapid mixing phase, imagnetic particle in slow mixing phase, and PAM at the last stage.

EXPERIMENT CONTENT

To observe the removal effect of metal ions by adding magnetic particle solely.

The objective of this test is to observe the removal effect of metal ions by adding magnetic particle solely. Select Zn^{2+} , Cu^{2+} , Pb^{+} as the targets to measure. The concentrations of $ZnSO_4$, $CuSO_4$ and $PbNO_3$ in raw water were 2 mg/L, 2 mg/L and 0.5 mg/L respectively.

As we can see from Figure 1, the removal rate of each index climb up with the adding of magnetic powder solely. Among them, the removal effect of Cu^{2+} is

best with the maximum removal rate up being 2.12%, Zn^{2+} secondly, with the maximum removal rate being 2.01%, Pb^{+} is the worst whose removal rate is 1.79%.

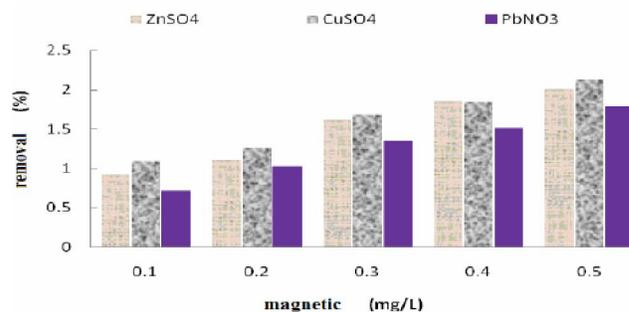


Figure 1 : The removal of the all parameters

Investigation PAC + magnetic powder + PAM for metal ions removal effect

Dissolve 2mg, 10mg and 20mg $ZnSO_4$ in 1L distilled water respectively to get $ZnSO_4$ solution, which fit for $CuSO_4$, and the quantity of $PbNO_3$ is not the same as, respectively, 0.5mg, 1mg, 2mg. Condition parameters in the test stay the same, namely 300r / m × 60s, 200R / m × 180s, 200R / m × 210s, then precipitate for 10min. In the slow mixing phase, magnetic particle

should be added, and the dosage is 0.5 g/L, PAC is 150 mg/L, and PAM is 2 mg/L. The removal effects are shown in TABLE 1.

We can get the conclusion from table 1 that the average removal effect of Zn²⁺, Cu²⁺ and Pb⁺ has kepted in 97% - 99% while Cu²⁺ > Pb⁺ > Zn²⁺. According to the "Cities Sewage Treatment Plant Pollutant Discharged Standard" (GB189182002) we can see that the project limit of Zn²⁺ is 1.0mg / L, Cu²⁺ is 0.5mg / L and Pb⁺ is

0.1mg / L. Visibly, Zn²⁺, Cu²⁺ and Pb⁺ can meet the project requirement in.

Study on removal efficiency on ZnSO₄ by diatomite and powder joint adding.

Select ZnSO₄ as the research object. The concentration of Zn²⁺(ZnSO₄) is below 1.0 mg/L at least.

In this stage the concrete removal rate on ZnSO₄ by diatomite and the concentration of ZnSO₄ in effluent are show in TABLE 2.

TABLE 1 : Removal efficiency on metal ions by PAC and PAM Joint adding

the indx measured	limit (mg/L)	raw water (mg/L)	effluent (mg/L)	removal rate (%)	row water (mg/L)	Effluent (mg/L)	removal rate(%)	Row water (mg/L)	Effluent (mg/L)	removal rate(%)
Zn ²⁺	1.0	2.0	0.0526	97.37	10	0.1726	98.27	20	0.5225	97.39
Cu ²⁺	0.5	2.0	0.0327	98.37	10	0.1422	98.59	20	0.4273	97.86
Pb ⁺	0.1	0.5	0.0117	97.66	1.0	0.0186	98.14	2.0	0.0392	98.04

TABLE 2 : Removal effect of ZnSO₄

Diatomite dosage (mg/L)		100	200	300	400	500	600
concentration of ZnSO ₄ in raw water 2mg/L	removal rate(%)	58.99	81.40	88.97	89.63	91.42	99.15
	effluent concentration (mg/L)	0.8201	0.3721	0.2207	0.2075	0.1716	0.0171
concentration of ZnSO ₄ in raw water 10mg/L	removal rate(%)	66.73	80.33	91.67	96.68	96.02	99.05
	effluent concentration (mg/L)	3.3266	1.9673	0.8326	0.4320	0.3979	0.0951
concentration of ZnSO ₄ in raw water 20mg/L	removal rate(%)	69.64	86.95	95.02	96.71	98.45	99.01
	effluent concentration (mg/L)	6.0726	2.6102	0.9952	0.6576	0.3102	0.1907

As show in TABLE 2, For raw water with ZnSO₄ concentration of 2mg / L, when the diatomite dose is 100mg / L, the project limit (1.0mg/L) of the "Cities Sewage Treatment Plant Pollutant Discharged Standard" can be meted. As the dosage increase to 600mg/L, the effluent concentration of ZnSO₄ reduced to 0.0171 mg/L, and the removal rate increased to 99.15%. For raw water with ZnSO₄ concentration of 10 mg/L or Zn²⁺ concentration of 20 mg/L the diatomite dose of 300 mg/L can meet the requirement. The diatomite dose of 600 mg/L can reduced raw water with ZnSO₄ concentration of 10 mg/L to 1.0 mg/L, and 20 mg/L to 0.2 mg/L.

Study on removal efficiency on CuSO₄ by diatomite and powder joint adding.

The removal efficiency of CuSO₄ by Diatomite is

similar to ZnSO₄. In this stage, taking CuSO₄ as the research object, the concentration of Cu²⁺ (CuSO₄) is below 0.5 mg/L. At least according to the "Cities Sewage Treatment Plant Pollutant Discharged Standard" (GB189182002).

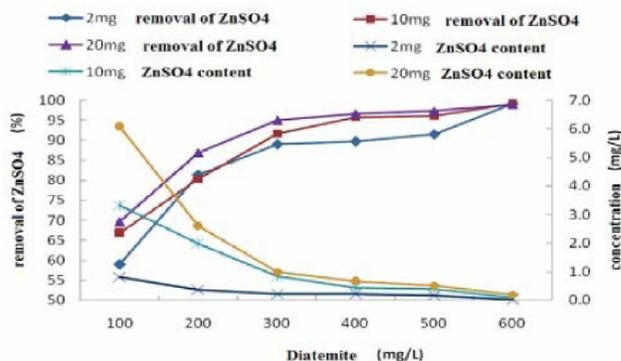


Figure 2 : The removal effect on ZnSO₄

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In this stage the concrete removal rate on CuSO_4 by diatomite and the concentration of CuSO_4 in effluent are show in TABLE 3.

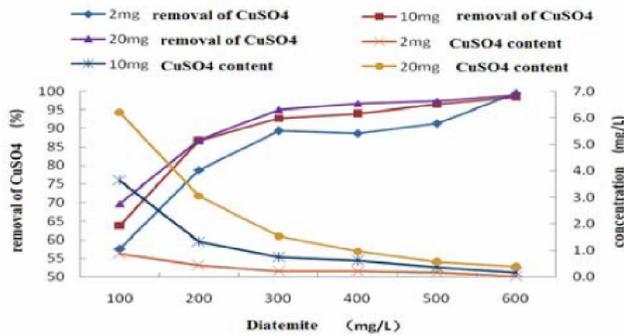


Figure 3 : Removal effect of CuSO_4

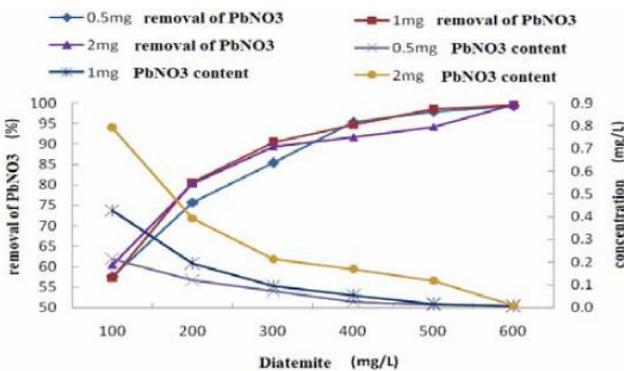


Figure 4 : Removal effect of PbNO_3

TABLE 3 : Removal effect of CuSO_4

Diatomite dosage (mg/L)		100	200	300	400	500	600
concentration of CuSO_4 in raw water 2mg/L	removal rate(%)	57.57	78.72	89.33	88.67	91.27	99.39
	effluent concentration (mg/L)	0.8487	0.4257	0.2135	0.2267	0.1746	0.0123
concentration of CuSO_4 in raw water 10mg/L	removal rate(%)	68.83	86.64	92.74	93.90	96.38	98.38
	effluent concentration (mg/L)	3.6172	1.3362	0.7259	0.6103	0.3625	0.1618
concentration of CuSO_4 in raw water 20mg/L	removal rate(%)	69.64	86.95	95.02	96.71	98.45	99.01
	Effluent concentration (mg/L)	6.2106	3.0578	1.5365	0.9618	0.5526	0.3829

TABLE 4 : Removal effect of PbNO_3

Diatomite dosage (mg/L)		100	200	300	400	500	600
concentration of PbNO_3 in raw water 0.5mg/L	removal rate (%)	57.48	75.75	85.39	95.44	97.95	99.24
	effluent concentration (mg/L)	0.2126	0.1213	0.0731	0.0228	0.0103	0.0038
concentration of PbNO_3 in raw water 1mg/L	removal rate (%)	57.21	80.68	90.38	94.64	98.61	99.45
	effluent concentration (mg/L)	0.4279	0.1932	0.0963	0.0536	0.0139	0.0056
concentration of PbNO_3 in raw water 2mg/L	removal rate (%)	60.49	80.37	89.37	91.64	94.19	99.59
	effluent concentration (mg/L)	0.7903	0.3926	0.2133	0.1673	0.0826	0.0082

From table4 we can see that only when the diatomite dosage reaches 500mg/L, can PbNO_3 concentration in effluent be controlled in 0.1mg/L (item limit), other

TABLE 3 shows that for raw water with CuSO_4 concentration of 2 mg/L, when the diatomite dose is 200 mg/L, the effluent water quality can meet the discharge standard(0.5mg/L) with the effluent concentration of 0.4257mg/L. As the dosage increases to 600 mg/L, the effluent concentration of ZnSO_4 reduced to 0.0123 mg/L.

Compared to ZnSO_4 the removal efficiency of CuSO_4 is slightly worse. But both of them can reach the removal rate of 99% in case that diatomite dosage reach 600 mg/L, In addition, to ensure the CuSO_4 effluent concentration of 0.5 mg/L, the diatomite dosage must reach 600 mg/L while diatomite dosage of 300 mg/L can do it to ZnSO_4 .

Study on removal efficiency on PbNO_3 by diatomite and powder joint adding.

In this stage, taking PbNO_3 as the research object, the concentration of Pb (PbNO_3) is below 0.1 mg/L at least according to the "Cities Sewage Treatment Plant Pollutant Discharged Standard" (GB189182002).

The concrete removal rate on PbNO_3 by diatomite and the concentration of PbNO_3 in effluent are show in TABLE 4.

dosage cannot satisfy the requirements.

Comparing the removal effect of these metal ions in case of the metal ion concentration of 2mg/L in raw

water, it can be concluded: that $Pb^{+} > Zn^{2+} > Cu^{2+}$, but there is so much difference.

CONCLUSIONS

For diatomite and powder joint adding, to meet the "Cities Sewage Treatment Plant Pollutant Discharged Standard" (GB189182002) that is the concentration of $CuSO_4$ in effluent is below 1.0 mg/L, $CuSO_4$ below 0.5 mg/L and $PbNO_3$ below 0.1 mg/L, the diatomite dosage should reach 300 mg/L, 600 mg/L and 500 mg/L respectively. When the diatomite dosage is 600 mg/L, the removal rate of each metal ion have reached 99%. The concentration of Zn^{2+} , Cu^{2+} and Pb^{+} in effluent can meet the "Cities Sewage Treatment Plant Pollutant Discharged Standard" (GB189182002) by PAC (150 mg/L) + powder (0.5 g/L) + PAM (2 mg/L) joint dosing in the condition parameters in the test.

REFERENCES

- [1] Hu Hui, Gao Hong, Jia Shao yi; Technology and Prospect of High-gradient Magnetic Filtration[J]. Environmental Science & Technology, **29(3)**, (2006).
- [2] Zheng Bisheng, Guo Siyuan, Lilin; Cai Miaoyan. Application of the high gradient magnetic separation technology processing molasses alcohol wastewater. Environmental science., **3**, (2004).
- [3] Sun Wei, Li Zhen, Wu Songhai, Jia Shaoyi. Magnetic separation technology in wastewater treatment of application. Magnetic materials and equipment, **04**, (2006).
- [4] Yang Zhan-li; Technical Analysis and Strategy Study on China's Urban Sewage Treatment [J]. Research of Environmental Sciences., **14(5)**, (2001).
- [5] Remark: Hebei University of Architecture Research Fund (Q-201309).