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Adsorption of rhodamine B by acid activated carbon-kinetic and thermodynamic studies

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ABSTRACT

A carbonaceous adsorbent prepared from an indigenous waste by acid treatment was tested for its efficiency in removing rhodamine B (RDB). The parameters studied include agitation time, initial dye concentration, carbon dose, pH and temperature. The adsorption followed first order reaction equation and the rate is mainly controlled by intra-particle diffusion. Freundlich and Langmuir isotherm models were applied to the equilibrium data. The adsorption capacity (Q_m) obtained from the Langmuir isotherm plots were 68.29, 68.21, 70.05 and 70.48 mg/g respectively at an initial pH of 7.0 at 30, 40, 50 and 60°C. The temperature variation study showed that the Rhodamine B adsorption is endothermic and spontaneous with increased randomness at the solid solution interface. Significant effect on adsorption was observed on varying the pH of the Rhodamine B solutions. Almost 62% removal of Rhodamine B was observed at 60°C. The Langmuir and Freundlich isotherms obtained, positive ΔH^0 value, pH dependent results and desorption of dye in mineral acid suggest that the adsorption of Rhodamine B on MCC involves physisorption mechanism.

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KEYWORDS

Activated carbon (MCC);
Rhodamine B (RDB);
Adsorption isotherm;
Equilibrium;
Kinetic;
Thermodynamic parameters;
Intraparticle diffusion;
Regeneration pattern.

INTRODUCTION

The discharge of highly coloured effluents into natural water bodies is not only aesthetically displeasing, but it also impedes light penetration, thus upsetting biological processes within a stream. In addition, many dyes are toxic to some organisms causing direct destruction of aquatic communities. Some dyes can cause allergic dermatitis, skin irritation, cancer and mutation in man^[1].

Wastewaters from dyeing industries released in to

nearby land or rivers without any treatment because the conventional treatment methods are not cost effective in the Indian context. Adsorption is one of the most effective methods and activated carbon is the preferred adsorbent widely employed to treat wastewater containing different classes of dyes, recognizing the economic drawback of commercial activated carbon^[1,2].

Many investigators have studied the feasibility of using inexpensive alternative materials like pearl millet husk, date pits, saw dust buffing dust of leather industry, coir pith, crude oil residue tropical grass, olive stone

and almond shells, pine bark, wool waste, coconut shell etc., as carbonaceous precursors for the removal of dyes from water and wastewater^[1,2,3].

The present study undertaken to evaluate the efficiency of a carbon adsorbent prepared from acid activated morinda coreia buch-ham bark carbon (MCC) carbon for removal of dye in aqueous solution. In order to design adsorption treatment systems, knowledge of kinetic and mass transfer processes is essential. In this paper, we have reported the applicability of kinetic and mass-transfer models for the adsorption of Rhodamine (B) onto acid activated carbon.

Adsorbent material

The dried morinda coreia buch-ham bark was carbonized with concentrated sulphuric acid in the weight ratio of 1:1(w/v). Heating for twelve hours in a furnace at 400°C has completed the carbonization and activation. The resulting carbon was washed with distilled water until a constant pH of the slurry was reached. Then the carbon was dried for four hours at 120°C in a hot air oven. The dried material was ground well to a fine powder and sieved.

Adsorption dynamic experiments

1. Batch equilibration method

The adsorption experiments were carried out in a batch process at 30, 40, 50 and 60°C temperatures. The known weight of adsorbent material was added to 50ml of the dye solutions with an initial concentration of 20mg/L to 100mg/L. The contents were shaken thoroughly using a mechanical shaker rotating with a speed of 120rpm. The solution was then filtered at preset time intervals and the residual dye concentration was measured.

2. Effect of variable parameters

2.1. Dosage of adsorbent

The various doses of the adsorbents are mixed with the dye solutions and the mixture was agitated in a mechanical shaker. The adsorption capacities for different doses were determined at definite time intervals by keeping all other factors constant.

2.2. Initial concentration of dye

In order to determine the rate of adsorption, ex-

periments were conducted with different initial concentrations of dyes ranging from 20 to 100mg/L. All other factors have kept constant.

2.3. Contact time

The effect of period of contact on the removal of the dye on adsorbent in a single cycle was determined by keeping particle size, initial concentration, dosage, pH and concentration of other ions constant.

2.4. pH

Adsorption experiments were carried out at pH 3,4,5,6,7,8,9 and 10. The acidic and alkaline pH of the media was maintained by adding the required amounts of dilute hydrochloric acid and sodium hydroxide solutions. The parameters like particle size of the adsorbents, dye concentration, dosage of the adsorbent and concentration of other ions have kept constant while carrying out the experiments. The pH of the samples was determined using a portable pH meter, Systronics make. The pH meter was calibrated with 4.0 and 9.2 buffers.

2.5. Chloride

The experiments were done in the presence of varying chloride environments using various sodium chloride solutions. While doing the experiments, the absence of other anions has ensured.

2.6. Temperature

The adsorption experiments were performed at four different temperatures viz., 30, 40, 50 and 60°C in a thermostat attached with a shaker, Remi make. The constancy of the temperature was maintained with an accuracy of $\pm 0.5^\circ\text{C}$.

2.7. Zero point charge

The pH at the potential of zero charge of the carbon (pHzpc) was measured using the pH drift method^[4]. The pH of the solution was adjusted by using 0.01M sodium hydroxide or hydrochloric acid. Nitrogen was bubbled through the solution at 25°C to remove the dissolved carbon dioxide. 50mg of the activated carbon was added to 50 ml of the solution. After stabilization, the final pH was recorded. The graphs of final pH versus initial pH used to determine the zero point charge of the activated carbon.

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2.8. Titration studies

According to Boehm^[4] only strong acidic carboxylic acid groups are neutralized by sodium bicarbonate, where as those neutralized by sodium carbonate are thought to be lactones, lactol and carboxyl group. The weakly acidic phenolic groups only react with strong alkali, sodium hydroxide. Therefore, by selective neutralization using bases of different strength, the surface acidic functional group in carbon can be characterized both quantitatively and qualitatively. Neutralization with hydrochloric acid characterizes the amount of surface basic groups that are, for example, pyrones and chromenes. The basic properties have described to surface basic groups and the pi electron system of carbon basal planes. The results indicate that the activated carbon used may possess acidic oxygen functional group on their surface and this is supported well by their respective zeropoint charge values. The results obtained from the above characterization studies are given in the TABLE 1.

2.9. Desorption studies

Desorption studies help to elucidate the nature of adsorption and recycling of the spent adsorbent and the dye. The effect of various reagents used for desorption are studied.

RESULTS AND DISCUSSIONS

Characterization of the adsorbent

Activated carbons are a widely used adsorbent due to its high adsorption capacity, high surface area, micro porous structure and high degree of surface respectively. The wide usefulness of carbon is a result of their specific surface area, high chemical and mechanical stability. The chemical nature and pore structure usually determines the sorption activity. The physico chemical properties are listed in TABLE 1

TABLE 1 : Characteristics of the adsorbent

Properties	MCC
Particle size (mm)	0.055
Density (g/cc)	0.3575
Moisture content (%)	2.25
Loss on ignition (%)	82
Acid insoluble matter (%)	2.5
Water soluble matter (%)	0.32
pH of aqueous solution	6.85
pH _{zpc}	6.35
Surface groups (m equiv/g)	
(i) Carboxylic acid	0.325
(ii) Lactone, lactol	0.049
(iii) Phenolic	0.061
(iv) Basic(pyrones and chromenes)	0.036

Effect of contact time and initial dye concentration

The experimental results of adsorptions of at various concentrations (20, 40, 60, 80 and 100mg/L) with contact time are shown in representative figure 1. The equilibrium data were collected in TABLE 2 reveals that, percent adsorption decreased with increase in initial dye concentration, but the actual amount of dye adsorbed per unit mass of carbon increased with increase in dye concentration. It means that the adsorp-

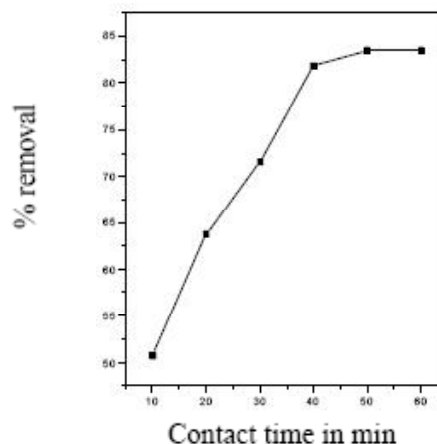


Figure 1 : Effect of contact time on the adsorption of rhodamine B[RDB]=40mg/L; pH=7; Adsorbent dose=50mg/50 ml

TABLE 2 : Equilibrium parameters for the adsorption of Dye onto activated carbon

[RDB] ₀	C _e (mg / L)				Q _e (mg/g)				Dye removed (%)			
					Temperature (C)							
	30°	40°	50°	60°	30°	40°	50°	60°	30°	40°	50°	60°
20	1.2756	1.0424	0.8547	0.6858	18.7244	18.9576	19.1453	19.3142	93.6	94.7	95.7	96.5
40	6.5842	6.1175	5.7686	5.3515	33.4158	33.8825	34.2314	34.6485	83.5	84.7	85.5	86.6
60	16.8765	16.2546	15.6441	15.0725	43.1235	43.7454	44.3559	44.9275	71.8	72.9	73.9	74.8
80	25.5045	24.9005	24.2156	23.5545	54.4955	55.0995	55.7844	56.4452	68.1	68.8	69.7	70.5
100	38.6754	37.8547	35.0052	34.2699	61.3246	62.1453	64.9948	65.7301	61.3	62.1	64.9	65.7

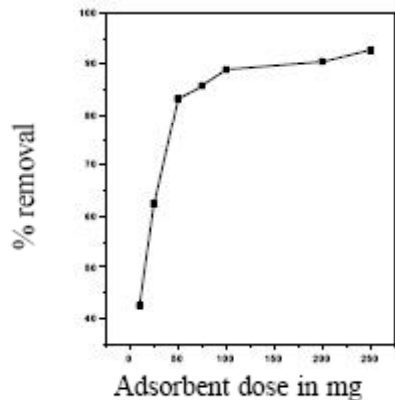


Figure 2 : Effect of adsorbent dose on the adsorption of rhodamine B [RDB]=40mg/L; pH=7; Contact time=60min

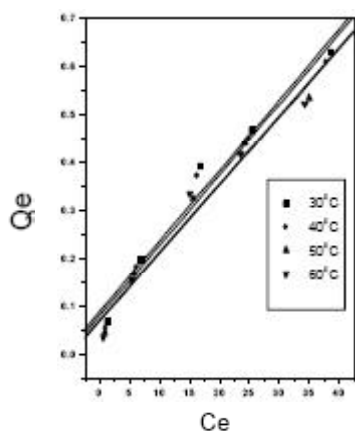


Figure 3 : Langmuir isotherm for the adsorption of rhodamine B

TABLE 3 : Langmuir isotherm results

Dye	Temp °C	Statistical parameters/constants		
		r ²	Q _m	b
RDB	30	0.9862	68.29	0.1615
	40	0.9861	68.21	0.1814
	50	0.9864	70.05	0.2020
	60	0.9802	70.48	0.2061

TABLE 4 : Dimensionless separation factor (R_L)

[RDB] ₀ (mg/L)	Temperature (°C)			
	30	40	50	60
20	0.236	0.216	0.198	0.195
40	0.134	0.121	0.110	0.108
60	0.093	0.084	0.076	0.074
80	0.072	0.064	0.058	0.057
100	0.058	0.052	0.058	0.057

tion is highly dependent on initial concentration of dye. It is because of that at lower concentration, the ratio of the initial number of dye molecules to the available surface area is low subsequently the fractional adsorption becomes independent of initial concentration. However,

at high concentration the available sites of adsorption becomes fewer and hence the percentage removal of dye is dependent upon initial concentration^[5,6]. Equilibrium have established at 40 minutes for all concentrations. Figure 1 reveals that the curves are single, smooth, and continuous, leading to saturation, suggesting the possible monolayer coverage of the dyes on the carbon surface.

Effect of carbon concentration:

The adsorption of the dyes on carbon was studied by varying the carbon concentration (10-250mg/50 ml) for 40mg/L of dye concentration. The percent adsorption increased with increase in the carbon concentration (Figure 2). This was attributed to increased carbon surface area and availability of more adsorption sites^[5,6]. Hence the remaining parts of the experiments are carried out with the adsorbent dose of 50mg/50ml.

Adsorption isotherm

The experimental data analyzed according to the linear form of the Langmuir and Freundlich isotherms^[7,8]. The Langmuir isotherm represented by the following equation

$$C_e/Q_e = 1/Q_m b + C_e/Q_m$$

where C_e is the equilibrium concentration (mg/L), Q_e is the amount adsorbed at equilibrium (mg/g) and Q_m and b is Langmuir constants related to adsorption efficiency and energy of adsorption, respectively. The linear plots of C_e/Q_e versus C_e suggest the applicability of the Langmuir isotherms (Figure 3). The values of Q_m and b were determined from slope and intercepts of the plots and are presented in TABLE 3. From the results, it is clear that the value of adsorption efficiency Q_m and adsorption energy b of the carbon increases on increasing the temperature. From the values we can conclude that the maximum adsorption corresponds to a saturated monolayer of adsorbate molecules on adsorbent surface with constant energy and no transmission of adsorbate in the plane of the adsorbent surface. The observed b values shows that the adsorbent prefers to bind acidic ions and that speciation predominates on sorbent characteristics, when ion exchange is the predominant mechanism takes place in the adsorption of RDB, it confirms the endothermic nature of the process involved in the system^[9,10,11]. To confirm the favourability

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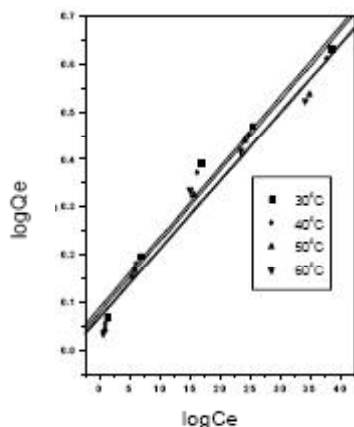


Figure 4 : Freundlich isotherm for the adsorption of rhodamine B

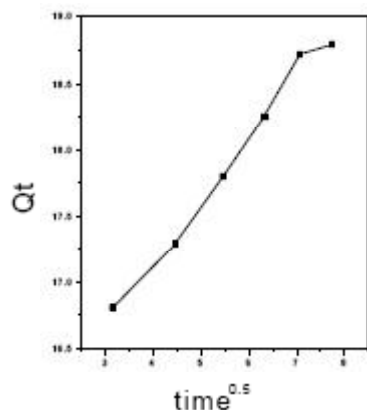


Figure 5 : Intraparticle diffusion effect [RDB]=10mg/L;pH=7; Adsorbent dose=50mg/50ml; Contact time=60 min

TABLE 5: Freundlich isotherm results

Dye	Temp °C	Statistical parameters/constants		
		r ²	Q _m	b
RDB	30	0.9973	1.4135	2.8892
	40	0.9972	1.3891	3.0425
	50	0.9952	1.3789	3.1121
	60	0.9946	1.3568	3.2768

of the adsorption process, the separation factor (R_L) was calculated and presented in TABLE 4. The values were found to be between 0 and 1 and confirm that the ongoing adsorption process is favorable^[12].

The Freundlich equation was employed for the adsorption of Rhodamine B dye on the adsorbent. The Freundlich isotherm was represented by

$$\log Q_e = \log K_f + 1/n \log C_e$$

where Q_e is the amount of Rhodamine B dye adsorbed (mg/g), C_e is the equilibrium concentration of dye in solution (mg/L) and K_f and n are constants incorporat-

ing the factors affecting the adsorption capacity and intensity of adsorption, respectively. Linear plots of $\log Q_e$ versus $\log C_e$ shows that the adsorption of Rhodamine B dye obeys the Freundlich adsorption isotherm (Figure 4). The values of K_f and n given in the TABLE 5 shows that the increase in negative charges on the adsorbent surface that makes electrostatic force like Vanderwaal's between the carbon surface and dye ion. The molecular weight, size and radii either limit or increase the possibility of the adsorption of the dye onto adsorbent. However, the values clearly show the dominance in adsorption capacity. The intensity of adsorption is an indicative of the bond energies between dye and adsorbent and the possibility of slight chemisorptions rather than physisorption^[10,11]. However, the multilayer adsorption of RDB through the percolation process may be possible. The values of n is greater than one indicating the adsorption is much more favorable^[12].

Effect of temperature

The adsorption capacity of the carbon increased with increase in the temperature of the system from 30°C-60°C. Thermodynamic parameters such as change in free energy were determined using the following equations (ΔG°) (kJ/mol), enthalpy (ΔH°) (kJ/mol) and entropy (ΔS°) (J/K/mol) were determined using the following equations

$$K_0 = C_{\text{solid}}/C_{\text{liquid}}$$

$$\Delta G^\circ = -RT \ln K_0$$

$$\log K_0 = \Delta S^\circ / (2.303RT) - \Delta H^\circ / (2.303RT)$$

where K_0 is the equilibrium constant, C_{solid} is the solid phase concentration at equilibrium (mg/L), C_{liquid} is the liquid phase concentration at equilibrium (mg/L), T is the temperature in Kelvin and R is the gas constant. The ΔH° and ΔS° values obtained from the slope and intercept of Van't Hoff plots have presented in TABLE 6. The values ΔH° are within the range of 1 to 93 kJ/mol indicates the physisorption. From the results we could make out that physisorption is much more favorable for the adsorption of RDB. The positive values of ΔH° show the endothermic nature of adsorption and it governs the possibility of physical adsorption^[11,13]. Because in the case of physical adsorption, while increasing the temperature of the system, the extent of dye adsorption increases, this rules out the possibility of chemisorption^[13]. The low ΔH° value depicts dye is

TABLE 6: Equilibrium constant and thermodynamic parameters for the adsorption of rhodamine B dye onto carbon

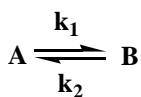
[D] ₀	K ₀				ΔG°				ΔH°	ΔS°
	Temperature (C)									
	30°	40°	50°	60°	30°	40°	50°	60°		
20	14.67	18.95	22.40	28.20	-6.76	-7.65	-8.34	-8.96	17.66	80.64
40	5.07	5.53	5.93	6.47	-4.09	-4.45	-4.78	-5.01	22.06	82.66
60	2.55	2.69	2.83	2.98	-2.63	-2.57	-2.81	-2.93	4.32	22.06
80	2.13	2.21	2.23	2.39	-1.91	-2.06	-2.15	-2.36	3.02	16.21
100	1.58	1.64	1.85	1.91	-1.16	-1.28	-1.64	-1.74	2.76	12.73

physisorbed onto adsorbent MCC.

The negative values of ΔG° (TABLE 6) shows the adsorption is highly favorable and spontaneous. The positive values of ΔS° (TABLE 6) shows the increased disorder and randomness at the solid solution interface of RDB with MCC adsorbent, while the adsorption there are some structural changes in the dye and the adsorbent occur. The adsorbed water molecules, which have displaced by the adsorbate species, gain more translational entropy than is lost by the adsorbate molecules, thus allowing the prevalence of randomness in the system. The enhancement of adsorption capacity of the activated carbon at higher temperatures was attributed to the enlargement of pore size and activation of the adsorbent surface^[12,13,14].

Kinetics of adsorption

The kinetics of sorption describes the solute uptake rate, which in turn governs residence time or sorption reaction. It is one of the important characteristics in defining the efficiency or sorption. In the present study, the kinetics of the dye removal was carried out to understand the behaviour of these low cost carbon adsorbents. The adsorption of dye from an aqueous follows reversible first order kinetics, when a single species are considered on a heterogeneous surface. The heterogeneous equilibrium between the dye solutions and the activated carbon are expressed as



where k₁ is the forward rate constant and k₂ is the backward rate constant. A represents dyes remaining in the aqueous solution and B represent dye adsorbed on the surface of activated carbon. The equilibrium constant (K₀) is the ration of the concentration adsorbate in adsorbent and in aqueous solution (K₀=k₁/k₂).

In order to study the kinetics of the adsorption pro-

cess under consideration the following kinetic equation proposed by Natarajan and Khalaf as cited in literature has been employed^[1].

$$\log C_0/C_t = (K_{ad}/2.303)t$$

Where C₀ and C_t are the concentration of the dye in (in mg/L) at time zero and at time t, respectively. The rate constants (K_{ad}) for the adsorption processes have been calculated from the slope of the linear plots of log C₀/C_t versus t for different concentrations and temperatures. The determination of rate constants as described in literature given by

$$K_{ad} = k_1 + k_2 = k_1 + (k_1/K_0) = k_1[1 + 1/K_0]$$

The overall rate constant k_{ad} for the adsorption of dye at different temperatures are calculated from the slopes of the linear Natarajan-Khalaf plots. The rate constant values are collected in TABLE 7 shows that the rate constant (k_{ad}) increases with increase in temperature suggesting that the adsorption process in endothermic in nature. Further, k_{ad} values decrease with increase in initial concentration of the dye. In cases of strict surface adsorption a variation of rate should be proportional to the first power of concentration. However, when pore diffusion limits the adsorption process, the relationship between initial dye concentration and rate of reaction will not be linear. Thus, in the present study pore diffusion limits the overall rate of dye adsorption. The over all rate of adsorption is separated into the rate of forward and reverse reactions using the above equation. The rate constants for the forward and reverse processes are also collected in TABLE 7 indicate that, at all initial concentrations and temperatures, the forward rate constant is much higher than the reverse rate constant suggesting that the rate of adsorption is clearly dominant^[11,13].

Intraparticle diffusion

The most commonly used technique for identifying the mechanism involved in the sorption process is by fitting the experimental data in an intraparticle diffusion

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TABLE 7 : Rate constants for the adsorption of rhodamine B dye ($10^3 k_{ad}$, min^{-1}) and the constants for forward ($10^3 k_1$, min^{-1}) and reverse ($10^3 k_2$, min^{-1}) process

[D] ₀	Temperature (C)											
	k_{ad}				30		40		50		60	
	30°	40°	50°	60°	K_1	K_2	K_1	K_2	K_1	K_2	K_1	K_2
20	1016.79	1432.37	1988.87	2831.95	951.94	64.85	1360.60	71.77	1903.88	84.99	2734.98	96.97
40	184.47	211.57	235.91	271.01	154.11	30.36	179.22	32.35	201.89	34.02	234.76	36.25
60	66.57	71.80	77.33	82.97	47.85	18.72	52.35	19.45	57.17	20.16	62.13	20.84
80	52.53	54.99	58.03	61.21	35.79	16.74	37.88	17.11	40.07	17.96	43.19	18.02
100	36.15	37.60	43.91	45.69	22.17	13.98	23.37	14.23	28.54	15.37	30.04	15.65

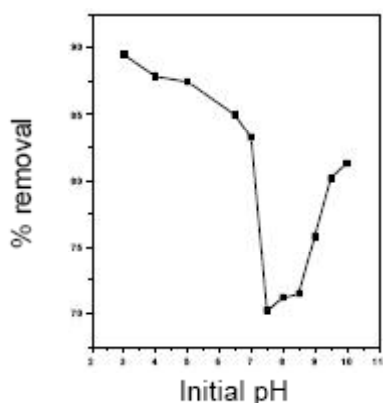


Figure 6 : Effect of initial pH on the adsorption of rhodamine B [RDB]=40mg/L; Adsorbent dose=50 mg/50ml; Contact time=60 min

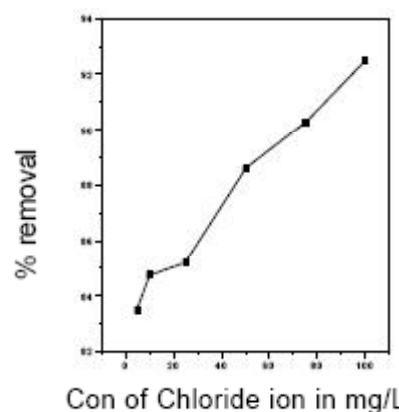


Figure 7 : Effect of other ions on the adsorption of rhodamine B [RDB]=40mg/L; pH=7; Adsorbent dose=50 mg/50ml

plot. Previous studies by various researchers showed that the plot of Q versus $t^{0.5}$ represents multi linearity, which characterizes the two or more steps involved in the sorption process. According to Weber and Morris, an intraparticle diffusion coefficient K_p is defined by the equation:

$$K_p = Q/t^{0.5}$$

Thus the K_p ($\text{mg/g min}^{0.5}$) value can be obtained from the slope of the plot of Qt (mg/g) versus $t^{0.5}$ for Rhodamine B. From figure 5, it was noted that the sorption process tends to be followed by two phases. The two phases in the intraparticle diffusion plot suggest that the sorption process proceeds by surface sorption and intraparticle diffusion^[15,16]. The initial curved portion of the plot indicates a boundary layer effect while the second linear portion is due to intraparticle or pore diffusion. The slope of the second linear portion of the plot has been defined as the intraparticle diffusion parameter K_p ($\text{mg/g min}^{0.5}$). On the other hand, the intercept of the plot reflects the boundary layer effect. The larger the intercept, the greater the contribution of the surface sorption in the rate limiting step. The calculated

intraparticle diffusion coefficient K_p value was given by 0.488, 0.542, 0.612, 0.675 and 0.739 $\text{mg/g min}^{0.5}$ for initial dye concentration of 20, 40, 60, 80 and 100 mg/L at 30°C.

Effect of pH

pH is one of the most important parameters controlling the adsorption process. The effect of pH of the solution on the adsorption of RDB ions on MCC was determined. The result is shown in figure 6. The pH of the solution was controlled by the addition of HCl or NaOH. The uptake of RDB ions at pH 7.5 was the minimum and a maximum in uptake was obtained at pH 3.0-6.5. However, when the pH of the solution was increased (more than pH 8), the uptake of RDB ions was increased. It appears that a change in pH of the solution results in the formation of different ionic species, and different carbon surface charge. At pH values lower than 6.5, the RDB ions can enter into the pore structure. At a pH value higher than 7.5, the zwitterions form of RDB in water may increase the aggregation of RDB to form a bigger molecular form (dimer) and become unable to enter into the pore structure of the carbon surface. The greater aggregation

of the zwitterionic form is due to the attractive electrostatic interaction between the carboxyl and xanthane groups of the monomer.

At a pH value higher than 8.5, the existence of OH⁻ creates a competition between -N⁺ and COO⁻ and it will decrease the aggregation of RDB, which causes an increase in the adsorption of RDB ions on the carbon surface. The effect of the charge on the carbon surface and the electrostatic force of attraction and repulsion between the carbon surface and the RDB ions cannot explain the result^[12,17].

Effect of the ionic strength on the adsorption of RDB on MCC

The effect of sodium chloride on the adsorption of RDB on MCC is shown in figure 7. In a low solution concentration NaCl had little influence on the adsorption capacity. At higher ionic strength the adsorption of RDB will be increased due to the partial neutralization of the positive charge on the carbon surface and a consequent compression of the electrical double layer by the Cl⁻ anion. The chloride ion can also enhance adsorption of RDB ion onto MCC by pairing of their charges and hence reducing the repulsion between the RDB molecules adsorbed on the surface. This initiates carbon to adsorb more of positive RDB ions^[1,17]

Desorption studies

Desorption studies help to elucidate the nature of adsorption and recycling of the spent adsorbent and the dye. If the adsorbed dyes can be desorbed using neutral pH water, then the attachment of the dye of the adsorbent is by weak bonds. If sulphuric acid or alkaline water desorb the dye then the adsorption is by ion exchange. If organic acids, like acetic acid can desorb the dye, then the dye is held by the adsorbent through chemisorption. The effect of various reagents used for desorption studies indicate that hydrochloric acid is a better reagent for desorption, because we could get more than 62% removal of adsorbed dye. The reversibility of adsorbed dye in mineral acid or base is in agreement with the pH dependent results obtained. The desorption of dye by mineral acids and alkaline medium indicates that the dyes were adsorbed onto the activated carbon through physisorption mechanisms^[12,18].

CONCLUSIONS

The experimental data correlated reasonably well by the Langmuir and Freundlich adsorption isotherms and the isotherm parameters were calculated. The low as well as high pH value pay the way to the optimum amount of adsorption of the dye. The amount of Rhodamine B adsorbed increased with increasing ionic strength and increased with increase in temperature. The dimensionless separation factor (R_L) showed that the activated carbon could be used for the removal of Rhodamine B from aqueous solution. The values of ΔH° , ΔS° and ΔG° results shows that the carbon employed has a considerable potential as an adsorbent for the removal of Rhodamine B.

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