



Trade Science Inc.

December 2007

Volume 2 Issue 3

CHEMICAL TECHNOLOGY

An Indian Journal

Full Paper

CTAIJ 2(3) 2007 [76-83]

Adsorption of ferrous ion by activated carbon-kinetic and equilibrium studies

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Received: 6th October, 2007 ; Accepted: 11th October, 2007

ABSTRACT

A carbonaceous adsorbent prepared from an indigenous waste, by acid treatment was tested for its efficiency in removing ferrous ion. The process parameters studied include agitation time, initial metal ion concentration, carbon dose, pH and temperature. The adsorption followed first order reaction equation and the rate is mainly controlled by intraparticle diffusion. Freundlich and Langmuir isotherm models were applied to the equilibrium data. The adsorption capacity (Q_m) obtained from the Langmuir isotherm plot were found to 42.52, 41.32, 39.84 and 38.71 mg/g at an initial pH of 7.0. The temperature variation study showed that the ferrous ions adsorption is endothermic and spontaneous with increased randomness at the solid solution interface. Significant effect on adsorption was observed on varying the pH of the ferrous ion solutions. The Langmuir and Freundlich adsorption isotherms obtained, positive ΔH^0 value, pH dependent results and desorption of metal ions in mineral acid suggest that the adsorption of ferrous ion on MCC involves chemisorption as well as physisorption mechanism. © 2007 Trade Science Inc. - INDIA

KEYWORDS

Activated carbon(MCC);
Ferrous ion;
Adsorption isotherm;
Equilibrium;
Kinetic and thermodynamic parameters;
Intraparticle diffusion;
Regeneration pattern.

INTRODUCTION

Toxic metal compounds coming to the earth's surface not only reach the earth's waters (seas, lakes, ponds and reservoirs) but can also contaminate ground water in trace amounts by leaching from the soil. Therefore, the earth's waters may contain various toxic metals.

Metal ion such ferrous produces undesirable effects on human and animal life even in low concentrations. In recent years many researchers have studied the removal of different heavy metal ions including chromium, nickel and copper from the water. Wastewaters from industries released in to nearby land or rivers without any treatment because the conventional treatment methods are not cost effective in the Indian context. On the other hand, low cost technologies never allow a

wishful metal ion removal and it has certain disadvantages. Adsorption is one of the most effective methods and activated carbon is the preferred adsorbent widely employed to treat wastewater containing different classes of metal ions recognizing the economic drawback of commercial activated carbon. Many investigators have studied the feasibility of using inexpensive alternative materials like pearl millet husk, date pits, saw dust buffing dust of leather industry, coir pith, crude oil residue tropical grass, olive stone and almond shells, pine bark, wool waste, coconut shell etc., as carbonaceous precursors for the removal of metal ion from water and wastewater^[1,2,3]. The present study undertaken to evaluate the efficiency of a carbon adsorbent prepared form acid activated morinda coreia buch-ham bark for the removal of ferrous ion aqueous solution. In

order to design adsorption treatment systems, knowledge of kinetic and mass transfer process is essential. In this paper, we have reported the applicability of kinetic and mass-transfer models for the adsorption of ferrous ion onto activated carbon

MATERIALS AND METHODS

Carbon was prepared by treating air-dried morinda coreia buch-ham bark (MCC) with con sulphuric acid in a weight ratio of 1:1. The resulting black product was kept in a furnace maintained at 500°C for 12 hours followed by washing with water until free from excess acid and dried at 150±5°C. The carbon product obtained was ground and the portion retained between 10 and 50µm sieves was used in all the experiments. All chemicals supplied by S.d. fine chemicals with high purity.

Batch equilibration method

All experiments were carried out at 30,40,50 and 60°C temperature in batch mode. Batch mode was selected because of its simplicity and reliability. The experiments were done in different Erlenmeyer glass flasks of 100ml capacity. Prior to each experiment, a predetermined amount of adsorbent was added to each flask. The stirring was kept constant (120rpm) for each run throughout the experiment to ensure equal mixing. Each flask was filled with a known volume of sample before commencing stirring such as metal solutions with an initial concentration of 10mg/L to 50mg/L. The flask containing the sample was withdrawn from the shaker at the predetermined time interval, filtered and the residual concentration of the ferrous ion was measured.

Effect of variable parameters

Dosage of adsorbents

Different doses consisting of 10 to 250mg/50ml of the adsorbent is mixed with the ferrous ion and the mixture was agitated in a mechanical shaker. The percentage of adsorption for different doses was determined by keeping all other factors constant.

Initial concentration

In order to determine the rate of adsorption, experiments were conducted with different initial concentrations of ferrous ions ranging from 10 to 50mg/L. All

other factors were kept constant.

Contact time

The effect of period of contact between the adsorbent and adsorbate on the removal of the ferrous ions in a single cycle was determined by keeping particle size, initial concentration, dosage, pH, and temperature constant.

Initial pH

Adsorption experiments were carried out at a range of pH of the solution i.e. 3-10. The acidic and alkaline pH of the medium was maintained by adding the required amounts of hydrochloric acid and sodium hydroxide solutions. The parameters like particle size of the adsorbent and temperature were kept constant while carrying out the experiments.

Other ions

Adsorption studies of a specific metal ion in the presence of chloride ions were experimentally verified using the adsorbents. This involved the determination of the percentage of ferrous ion adsorbed from 30mg/L of initial concentration of the ferrous ion solution with varying concentration of the added ion keeping all other factors constant.

Temperature

The adsorption experiments were performed at four different temperatures viz., 30, 40, 50 and 60°C in a thermostated shaker machine (Remi, India). The constancy of the temperature was maintained with an accuracy of ±0.5°C.

Zero point charge

The pH at the potential of zero charge of the carbon (pH_{zpc}) was measured using the pH drift method. The pH of the solution was adjusted by using 0.01 M sodium hydroxide or hydrochloric acid. Nitrogen was bubbled through the solution at 25°C to remove the dissolved carbon dioxide. 50 mg of the activated carbon was added to 50 ml of the solution. After stabilization, the final pH was recorded. The graphs of final pH versus initial pH used to determine the zero point charge of the activated carbon^[4].

Titration studies

According to Boehm^[4] only strong acidic carboxy-

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TABLE 1: Equilibrium parameters for the adsorption metal ion onto MCC

Ferrous ion	C_e (mg/L)				Q_e (mg/g)				Metal ions removed (%)			
	30°C	40°C	50°C	60°C	30°C	40°C	50°C	60°C	30°C	40°C	50°C	60°C
10	1.8572	1.6485	1.4528	1.2621	8.1428	8.3515	8.5472	8.7379	81.43	83.51	85.47	87.37
20	4.2856	3.9059	3.6124	3.3059	15.7144	16.30941	16.3876	16.6941	78.57	80.47	81.93	83.47
30	8.5425	8.1339	7.7291	7.4199	21.4575	21.8661	22.2709	22.5801	71.52	72.88	74.23	75.26
40	13.6550	13.1452	13.6387	13.5288	26.3450	26.8548	26.3613	26.4712	65.86	67.13	65.90	66.17
50	19.2575	18.6798	18.0622	17.6017	30.7425	31.3202	31.9378	32.3983	61.48	62.64	63.87	64.79

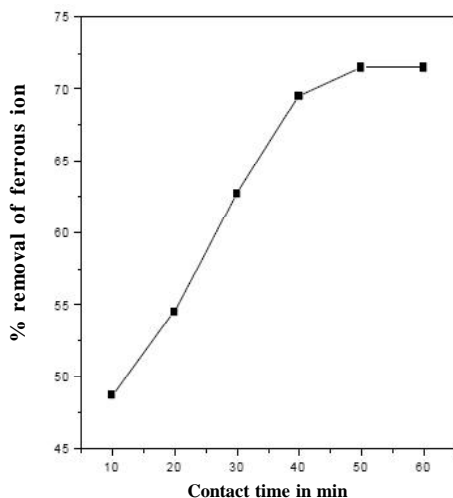


Figure 1 : Effect contact time on the adsorption of ferrous ion [Fe]=30mg/L; Adsorbent dose= 50mg/50ml; pH=7

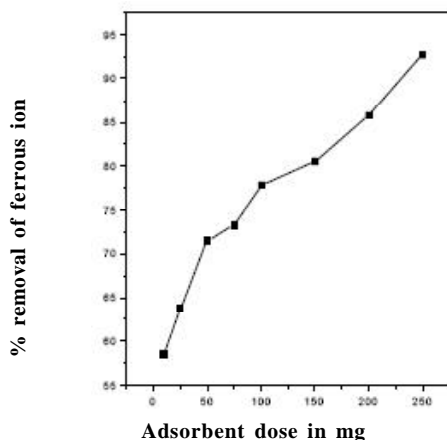


Figure 2 : Effect of adsorbent dose on the adsorption of ferrous ion [Fe]=30mg/L; Adsorbent dose=50mg/50ml; pH=7

lic acid groups are neutralized by sodium bicarbonate, where as those neutralized by sodium carbonate are thought to be lactones, lactol and carboxyl group. The weakly acidic phenolic groups only react with strong alkali, sodium hydroxide. Therefore, by selective neutralization using bases of different strength, the surface acidic functional group in carbon can be characterized both quantitatively and qualitatively. Neutralization with

hydrochloric acid characterizes the amount of surface basic groups that are, for example, pyrones and chromenes. The basic properties have described to surface basic groups and the pi electron system of carbon basal planes. The results indicate that the activated carbon used may possess acidic oxygen functional group on their surface and this is supported well by their respective zero point charge values. The results obtained from the above characterization studies are given in the results and discussions part.

Regeneration studies

The regeneration of the adsorbed carbon is done by using 0.2M mineral acids and sodium chloride solutions.

RESULT AND DISCUSSION

Characterization of the adsorbent

Activated carbons are a widely used adsorbent due to its high adsorption capacity, high surface area, micro porous structure and high degree of surface respectively. The wide usefulness of carbon is a result of their specific surface area, high chemical and mechanical stability. The chemical nature and pore structure usually determines the sorption activity. The physico chemical properties of the chosen adsorbent are listed below

Characteristics of the adsorbent

Properties	MCC
Particle size (mm)	0.055
Density (g/cc)	0.3575
Moisture content (%)	2.25
Loss on ignition (%)	82
Acid insoluble matter (%)	2.5
Water soluble matter (%)	0.32
pH of aqueous solution	6.85
pH_{zpc}	6.35
Surface groups (m equiv/g)	
(i) Carboxylic acid	0.325
(ii) Lactone, lactol	0.049
(iii) Phenolic	0.061
(iv) Basic (pyrones and chromenes)	0.036

TABLE 2 : Langmuir isotherm results

(metal ion)	Temp (°C)	Statistical parameters		Constants b
		r ²	Q _m	
Ferrous ion adsorption	30°	0.9972	42.52	0.13
	40°	0.9934	41.32	0.15
	50°	0.9905	39.85	0.18
	60°	0.9879	38.79	0.21

TABLE 3: Dimensionless separation factor (R_L)

Ferrous ion (mg/L)	Temperature (°C)			
	30°C	40°C	50°C	60°C
10	0.440	0.400	0.359	0.321
20	0.282	0.250	0.218	0.191
30	0.207	0.181	0.157	0.136
40	0.164	0.142	0.122	0.105
50	0.135	0.117	0.101	0.086

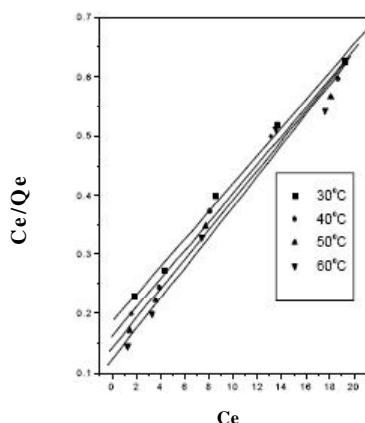


Figure 3 : Langmuir isotherm for the adsorption of ferrous ion

Effect of contact time and initial ferrous ion concentration

The experimental results of adsorptions of ferrous ion on the activated carbon at various concentrations (10,20,30,40 and 50mg/L) with contact time are shown in figure 1. The equilibrium data were collected in TABLE 1 reveals that, percent adsorption decreased with increase in initial ferrous ion concentration, but the actual amount of ferrous ion adsorbed per unit mass of carbon increased with increase in metal ion concentration. It means that the adsorption is highly dependent on initial concentration of ferrous ion. It is because of that at lower concentration, the ratio of the initial number of ferrous ion to the available surface area is low subsequently the fractional adsorption becomes independent of initial concentration. However, at high concentration the available sites of adsorption becomes fewer and hence the percentage removal of ferrous ion

is dependent upon initial concentration. Equilibrium have established at 40 minutes for all concentrations. Figure 2 reveals that the curves are single, smooth, and continuous, leading to saturation, suggesting the possible monolayer coverage of the ferrous ion on the carbon surface^[5,6].

Adsorption isotherm

The experimental data analyzed according to the linear form of the Langmuir^[7] and Freundlich^[8] isotherms.

The Langmuir isotherm represented by the following equation

$$C_e/Q_e = 1/Q_m b + C_e/Q_m \quad (1)$$

Where C_e is the equilibrium concentration(mg/L), Q_e is the amount adsorbed at equilibrium (mg/g) and Q_m and b is Langmuir constants related to adsorption efficiency and energy of adsorption, respectively. The linear plots of C_e/Q_e versus C_e suggest the applicability of the Langmuir isotherms(Figure 3). Values of Q_m and b were determined from slope and intercepts of the plots and are presented in TABLE 2. From the results, it is clear that the value of adsorption efficiency Q_m and adsorption energy b of the carbon increases on increasing the temperature. From the values we can conclude that the maximum adsorption corresponds to a saturated monolayer of adsorbate molecules on adsorbent surface with constant energy and no transmission of adsorbate in the plane of the adsorbent surface^[9,10]. The trend shows that the adsorbent prefers to bind acidic ions and that speciation predominates on sorbent characteristics, when ion exchange is the predominant mechanism. Further, it confirms the endothermic nature of the processes involved in the system. To confirm the adorability of the adsorption process, the separation factor (R_L) has calculated and presented in TABLE 3. The values were found to be between 0 and 1 and confirm that the ongoing adsorption process is favourable^[11]

The Freundlich equation have also employed for the adsorption of ferrous ion on the adsorbent. The Freundlich isotherm have represented as

$$\log Q_e = \log K_f + 1/n \log C_e \quad (2)$$

Where Q_e is the amount of ferrous ion adsorbed (mg/g), C_e is the equilibrium concentration of metal ion in solution(mg/L) and K_f and n are constants incorpo-

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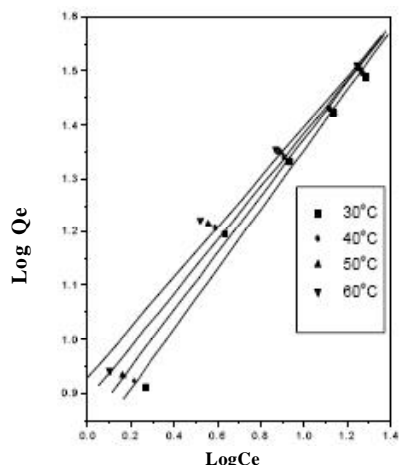


Figure 4 : Freundlich isotherm for the adsorption of ferrous ion

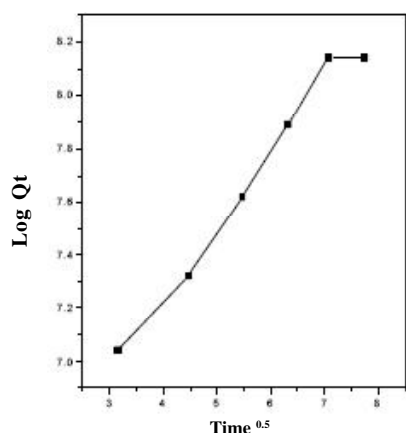


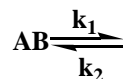
Figure 5 : Intraparticle diffusion effect for the adsorption of ferrous ion

rating all factors affecting the adsorption capacity and intensity of adsorption, respectively. Linear plot of $\log Q_e$ versus $\log C_e$ shows that the adsorption of ferrous ion follows the Freundlich isotherm (Figure 4). Values of K_f and n were found and given in the TABLE 4, shows the increase of negative charge on the surface that enhances the electrostatic force like Vanderwaal's between the carbon surface and metal ion, which in-

creases the adsorption of ferrous ion. The values clearly show that dominance in adsorption capacity. The intensity of adsorption is an indicative of the bond energies between ferrous ion and adsorbent and the possibility of slight chemisorptions rather than physisorption^[10,11]. The possibility of multilayer adsorption of metal ion through the percolation process cannot be ruled out. However, the values of n is greater than one indicating the adsorption is much more favourable^[12,13].

Kinetics of adsorption

Kinetics of sorption describes the solute uptake rate, which in turn governs the residence time of sorption reaction. It is one of the important characteristics in defining the efficiency of sorption. In the present study, the kinetics of the ferrous ion removal has carried out to understand the behaviour of this low cost carbon adsorbent. The adsorption of ferrous ion from an aqueous solution follows reversible first order kinetics, when a single species considered on a heterogeneous surface. The heterogeneous equilibrium between the ferrous ion solution and the activated carbon have expressed as



Where k_1 is the forward rate constant and k_2 is the backward rate constant. A represents ferrous ion remaining in the aqueous solution and B represents ferrous ion adsorbed on the surface of activated carbon.

TABLE 4: Freundlich isotherm results

(metal ion)	Temp (°C)	Statistical parameters		Constants	
		r^2	Q_m	b	
Ferrous ion adsorption	30°	0.9892	1.74	1.80	
	40°	0.9890	1.69	1.88	
	50°	0.9870	1.64	2.01	
	60°	0.9863	1.59	2.14	

TABLE 5 : Equilibrium constant and thermodynamic parameters for the adsorption of metal ions onto acid activated carbon temperature (°C)

Ferrousion (mg/L)	K_o 30°C	$-\Delta G^\circ$				$-\Delta H^\circ$				ΔS°
		40°C	50°C	60°C	30°C	40°C	50°C	60°C		
10	4.38	5.74	5.88	6.92	3.72	4.55	4.75	5.35	11.65	51.06
20	3.66	4.12	4.53	5.04	3.27	3.68	4.06	4.48	8.77	39.74
30	2.51	2.68	2.88	3.04	2.31	2.57	2.84	3.08	5.36	25.34
40	1.92	2.04	1.93	1.95	1.65	1.85	1.76	1.85	3.24	16.24
50	1.59	1.67	1.76	1.84	1.17	1.34	1.53	1.68	3.99	17.05

ΔH° (kJ/mol), ΔS° (J/K/mol), ΔG° (kJ/mol)

TABLE 6: Rate constants for the adsorption of ferrous ions ($10^3 k_{ad}$, min^{-1}) and the constants for forward ($10^3 K_1$, min^{-1}) and reverse ($10^3 K_2$, min^{-1}) process

Ferrous ion (mg/L)	Temperature ($^{\circ}\text{C}$)											
	k_{ad}				k_1		k_2		k_1		k_2	
	30 $^{\circ}\text{C}$	40 $^{\circ}\text{C}$	50 $^{\circ}\text{C}$	60 $^{\circ}\text{C}$	30 $^{\circ}\text{C}$	40 $^{\circ}\text{C}$	30 $^{\circ}\text{C}$	40 $^{\circ}\text{C}$	30 $^{\circ}\text{C}$	40 $^{\circ}\text{C}$	30 $^{\circ}\text{C}$	40 $^{\circ}\text{C}$
10	263.02	325.51	405.88	517.78	208.75	54.21	264.47	61.04	337.48	68.40	441.83	75.95
20	203.03	240.36	275.04	323.57	154.29	48.74	186.10	54.26	216.93	58.11	259.74	63.83
30	120.70	132.23	145.29	156.58	84.56	36.14	94.43	37.80	105.75	39.54	115.96	40.62
40	86.20	92.53	86.38	87.69	55.66	30.54	60.92	31.61	57.91	28.47	60.29	27.40
50	68.69	72.75	77.51	81.36	41.51	27.18	44.85	27.90	48.60	28.97	52.02	29.36

TABLE 7: Intraparticle diffusion (K_p)

[Ferrous ion] (mg/L)	K_p
10	0.283
20	0.305
30	0.332
40	0.358
50	0.386

The rate constants calculated as earlier^[11,12,13]. The data furnished in TABLE 6, is evident that the forward rate constant is much higher than the backward rate constant suggesting that the rate of adsorption is clearly dominant. At equilibrium, the rate is the ratio of the concentration of adsorbate in adsorbent and concentration of adsorbate in aqueous solution given by K_0 . The calculated values presented in the TABLE 5. The results indicates that K_0 values decreases with increase in the concentration of the ferrous ion and increases with increase in temperature

A clear examination of the effect of ferrous ion concentrations on the rate constant K_{ad} (TABLE 6), the values help to describe the mechanism of metal ion removal taking place. In cases of strict surface adsorption a variation of rate should be proportional to the first power of concentration. However, when pore diffusion limits the adsorption process, the relationship between initial ferrous ion concentration and rate of reaction will not be linear. It shows that pore diffusion limits the overall rate of ferrous ion adsorption^[12].

The contact-time experimental results can be used to study the rate-limiting step in the adsorption process, as shown by Weber and Morris^[13,14]. Since the particles are vigorously agitated during the adsorption period, it is probably reasonable to assume that the rate is not limited by mass transfer from the bulk liquid to the particle external surface, one might then postulate that the rate-limiting step may be either film or intraparticle diffusion. As they act in series, the slower of the two will be the rate-determining step^[13].

The rate constant for intraparticle diffusion is obtained using the equation

$$Q = K_p t^{1/2} + C \quad (3)$$

Here, K_p (mg/g/min) is the intraparticle diffusion rate constant. The K_p values obtained from the slope of the linear portions of the curves at metal ion concentration (Figure 5 & TABLE 7). The K_p values increased with increase in the ferrous ion concentration, which reveals that the rate of adsorption is governed by the diffusion of adsorbed ferrous ion within the pores of the adsorbent.

Effect of temperature

The adsorption capacity of the carbon increased with increase in the temperature of the system from 30 $^{\circ}\text{C}$ - 60 $^{\circ}\text{C}$. Thermodynamic parameters such as change in free energy (ΔG°), enthalpy (ΔH°) and entropy (ΔS°) were determined using the following equations^[11,12,15,16]

$$K_0 = C_{solid}/C_{liquid} \quad (4)$$

$$\Delta G^{\circ} = -RT \ln K_0 \quad (5)$$

$$\log K_0 = \Delta S^{\circ}/(2.303RT) - \Delta H^{\circ}/(2.303RT) \quad (6)$$

Where K_0 is the equilibrium constant, C_{solid} is the solid phase concentration at equilibrium (mg/L), C_{liquid} is the liquid phase concentration at equilibrium (mg/L), T is the temperature in Kelvin and R is the gas constant. The ΔH° and ΔS° values obtained from the slope and intercept of Van't Hoff plots have presented in TABLE 5. The values are within the range of 1 to 93KJ/mol indicates the favourability of physisorption. From the order we could make out physisorption is much more favourable for ferrous ion. The positive values of ΔH° show the endothermic nature of adsorption and it governs the possibility of physical adsorption. Because in the case of physical adsorption, while increasing the temperature of the system, the extent of metal ion adsorption increases, this rules out the possibility of

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chemisorptions. However, the very low ΔH° value depicts ferrous ion is physisorbed onto adsorbent^[12,13,15].

The negative values of ΔG° (TABLE 5) shows the adsorption is highly favourable for ferrous ion. However, it indicates that the metal ion adsorption was spontaneous. The positive values of ΔS° (TABLE 5) shows the increased disorder and randomness at the solid solution interface of with adsorbent MCC. While the adsorption there are some structural changes in the ferrous ion and the adsorbent occur. The adsorbed water molecules, which have displaced by the adsorbate species, gain more translational entropy than is lost by the adsorbate molecules, thus allowing the prevalence of randomness in the system^[5,12,18]. From the results, we could make out that more efficient physisorption. Enhancement of adsorption capacity of the activated carbon at higher temperatures has attributed to the enlargement of pore size and activation of the adsorbent surface^[11].

Effect of pH

The experiments carried out at different pH shows that there was a change in the percent removal of ferrous ion over the entire pH range of 3 to 10 shown in the Figure 6, pH is one of the most important parameters controlling the adsorption process. The effect of pH of the solution on the adsorption of ferrous ion on MCC was determined. The result is shown in figure 6. The pH of the solution was controlled by the addition

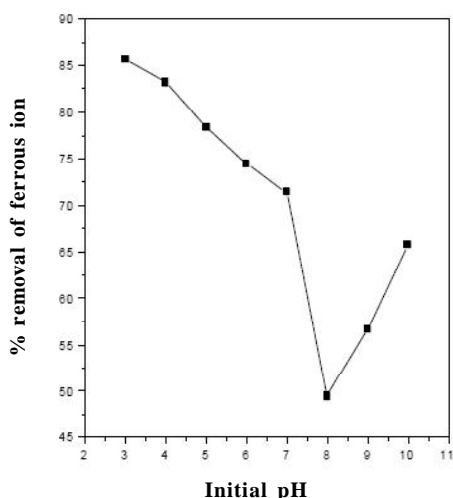


Figure 6 : Effect of initial pH on the adsorption of ferrous ion [Fe]=30mg/L; Adsorbent dose=50mg/50ml; contact time=60min

of HCl or NaOH. The uptake of ferrous ions at pH 8 was the minimum and a maximum in uptake was obtained at pH 3.0. However, when the pH of the solution was increased (more than pH 7), the uptake of ferrous ions was increased. It appears that a change in pH of the solution results in the formation of different ionic species, and different carbon surface charge. At pH values lower than 5, the ferrous ions can enter into the pore structure. At a pH value higher than 8, the zwitterions form of ferrous ion in water may increase the aggregation of ferrous ion to form a bigger molecular form(dimer) and become unable to enter into the pore structure of the carbon surface. The greater aggregation of the zwitterionic form is due to the attractive electrostatic interaction between the ionic groups of the monomer^[17].

At a pH value higher than 9, the existence of MCC surface OH⁻ creates a competition between ferrous ion and it will decrease the aggregation of ferrous, which causes an increase in the adsorption of ferrous ions on the carbon surface. The effect of the charge on the carbon surface and the electrostatic force of attraction and repulsion between the carbon surface and the ferrous ions cannot explain the outcome.

Effect of other ions

The effect of sodium chloride on the adsorption of ferrous ion on MCC is shown in. In a low solution concentration NaCl had little influence on the adsorption capacity. At higher ionic strength the adsorption of ferrous ion will be increased due to the partial neutralization of the positive charge on the carbon surface and a consequent compression of the electrical double layer by the Cl⁻ anion. The chloride ion can also enhance adsorption of ferrous ion onto MCC by pairing of their charges and hence reducing the repulsion between the ferrous ions adsorbed on the surface. This initiates carbon to adsorb more of positive ferrous ions^[17,18].

Desorption studies

Desorption studies help to elucidate the nature of adsorption and recycling of the spent adsorbent and the ferrous ion. If the adsorbed ferrous ion can be desorbed using neutral pH water, then the attachment of the ferrous ion of the adsorbent is by weak bonds. If sulphuric acid or alkaline water desorb the metal ion,

then the adsorption is by ion exchange. If organic acids, like acetic acid can desorb the ferrous ion, then the metal ion has held by the adsorbent through chemisorption. The effect of various reagents used for desorption studies indicate that hydrochloric acid is a better reagent for desorption, because we could get more than 70% removal of adsorbed ferrous ion. The reversibility of adsorbed metal ion in mineral acid or base is in agreement with the pH dependent results obtained. The desorption of ferrous ion by mineral acids and alkaline medium indicates that the ferrous ion was adsorbed onto the activated carbon through by physisorption mechanisms^[11,12,13,18].

CONCLUSIONS

The experimental data correlated reasonably well by the Langmuir and Freundlich adsorption isotherms and the isotherm parameters were calculated. The amount of ferrous ion adsorbed increased with increase in pH of the medium. The amount of ferrous ion adsorbed slightly decreased with increasing ionic strength and increased with increase in temperature. The dimensionless separation factor (R_L) showed that the activated carbon could be used for the removal of ferrous ion from aqueous solution. The values of ΔH° , ΔS° and ΔG° results shows that the carbon employed has a considerable potential as an adsorbent for the removal of ferrous ion.

ACKNOWLEDGEMENT

The authors acknowledge sincere thanks to Mrs. Mala Arivoli, The Principal, M.R. Government Arts College, Mannargudi and The Director of Collegiate Education, Chennai for carrying out this research work successfully.

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